

European Drag Reduction and Flow Control Meeting
Rome, Apr. 3-6, 2017

Direct Numerical Simulation of Drag Reduction with Uniform Blowing over a Two-dimensional Roughness

Eisuke Mori¹, Maurizio Quadrio² and Koji Fukagata¹

¹ Keio University, Japan

² Politecnico di Milano, Italy



Uniform blowing (UB)

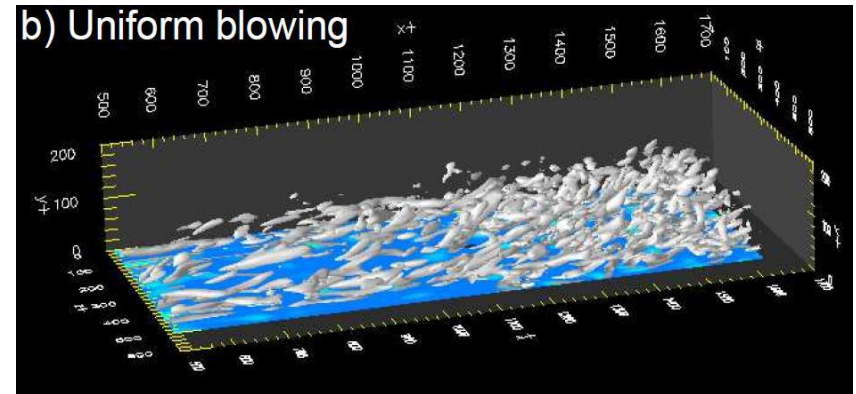
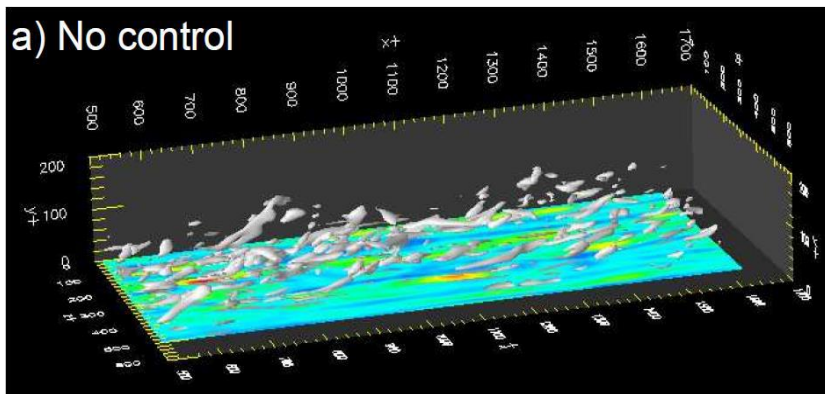
- Drag contribution in a channel flow with UB(/US)

$$C_f = \underbrace{\frac{12}{\text{Re}_b}}_{\text{Viscous Contribution}} + \underbrace{12 \int_0^2 (1-y)(-\overline{u'v'}) dy}_{\text{Turbulent contribution}} - \underbrace{12V_w \int_0^2 (1-y)\bar{u} dy}_{\text{Convective (=UB/US) contribution}}$$

V_w : Blowing velocity

(= laminar drag, **const.**) (Fukagata et al., *Phys. Fluids*, 2002)

- Excellent performance (about 45% by $V_w = 0.5\%U_\infty$)
- **Unknown over a rough wall** (Kametani & Fukagata, *J. Fluid Mech.*, 2011)



On a boundary layer, White: vortex core, Colors: wall shear stress

UB over a rough wall

Experimental results so far

- **Similar to the smooth-wall cases**
 - Schetz and Nerney, *AIAA J.*, 1977
 - Voisinet, 1979
- **Opposite behavior**
(drag increased, turbulent intensity suppressed)
 - Miller et al., *Exp. Fluids*, 2014

Contradicting remarks exist

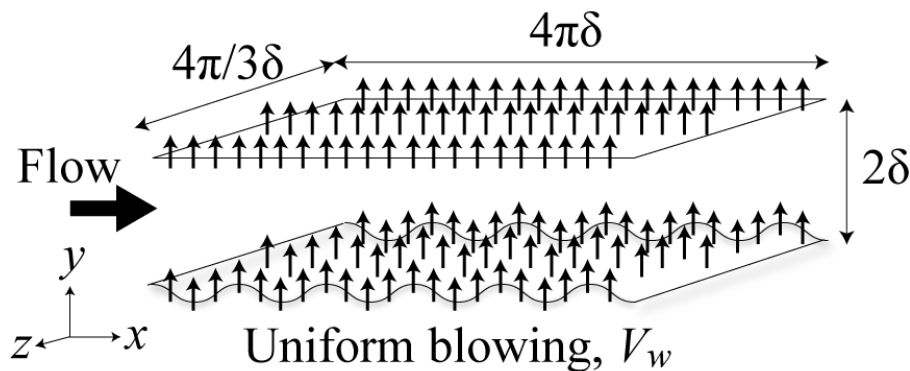
Goal

Investigate the interaction between roughness and UB for drag reduction using numerical simulation

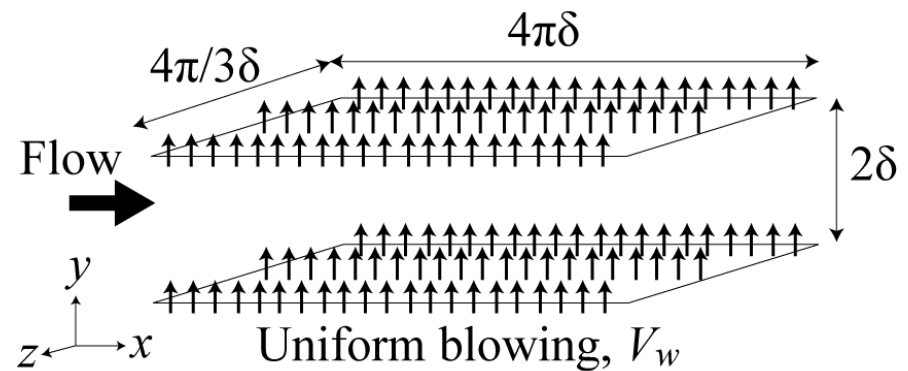
- DNS of turbulent channel flow
- Drag reduction **performance** and **mechanism**
- **Combined effect** of UB and roughness

Numerical procedure

- **Based on FD code** (for wall deformation)
(Nakanishi et al., *Int. J. Heat Fluid Fl.*, 2012)
- **Constant flow rate**, $Re_b = 2U_b\delta/\nu = 5600$
 - so that $Re_\tau \approx 180$ in a plane channel (K.M.M.)
- $\Delta x^+ = 4.4$, $0.93 < \Delta y^+ < 6$, $\Delta z^+ = 5.9$
- **UB magnitude**: $V_w/U_b = 0, 0.1\%, 0.5\%, 1\%$



ROUGH CASE



SMOOTH CASE

Model of rough wall

Roughness displacement

$$d(x) = \delta \sum_{i=1}^8 A_i \sin\left(\frac{2i\pi x}{L_x/2}\right)$$

(E. Napoli et al., *J. Fluid Mech.*, 2008)

δ : channel half height

L_x : Channel length, $4\pi\delta$

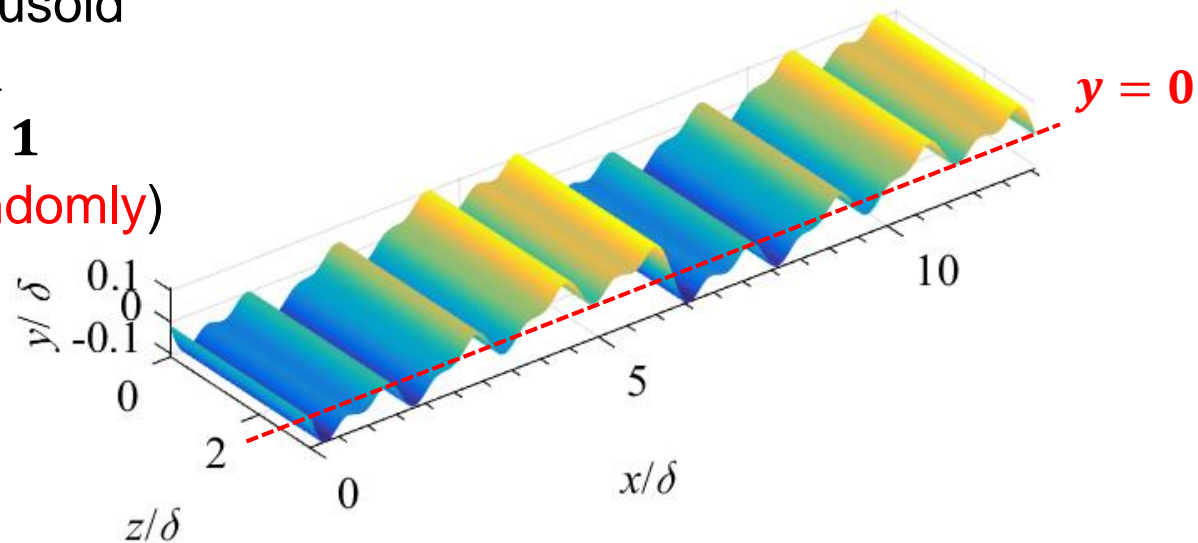
A_i : Amplitude of each sinusoid

$$A_i = \begin{cases} 1, & \text{for } i = 1 \\ [0, 1], & \text{for } i \neq 1 \end{cases}$$

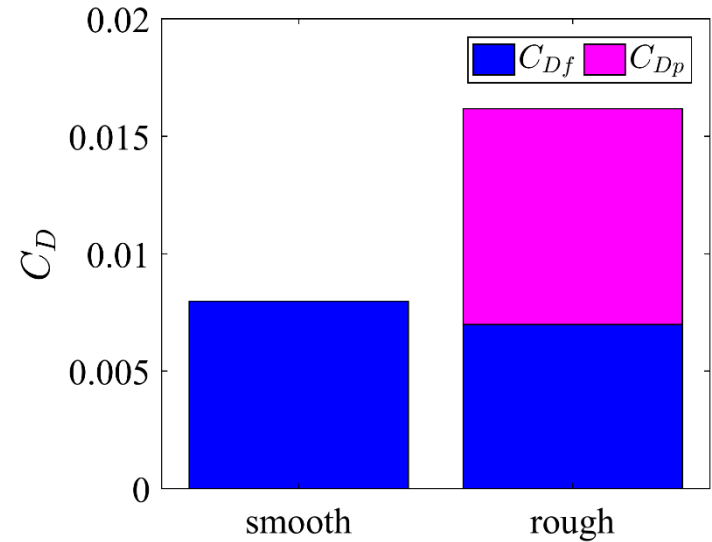
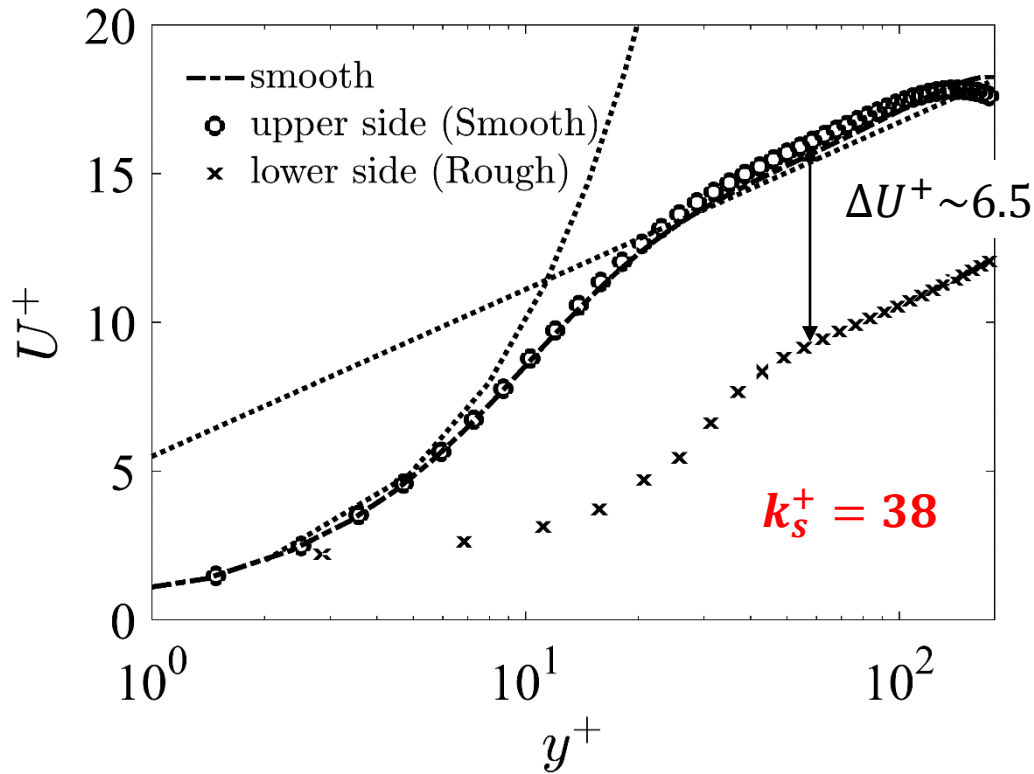
(Defined **randomly**)

with rescaling so that
 $\overline{|d(x)|} = 0.05\delta$

$$|d(x)|_{\max} = 0.11\delta$$



The result of the base flow



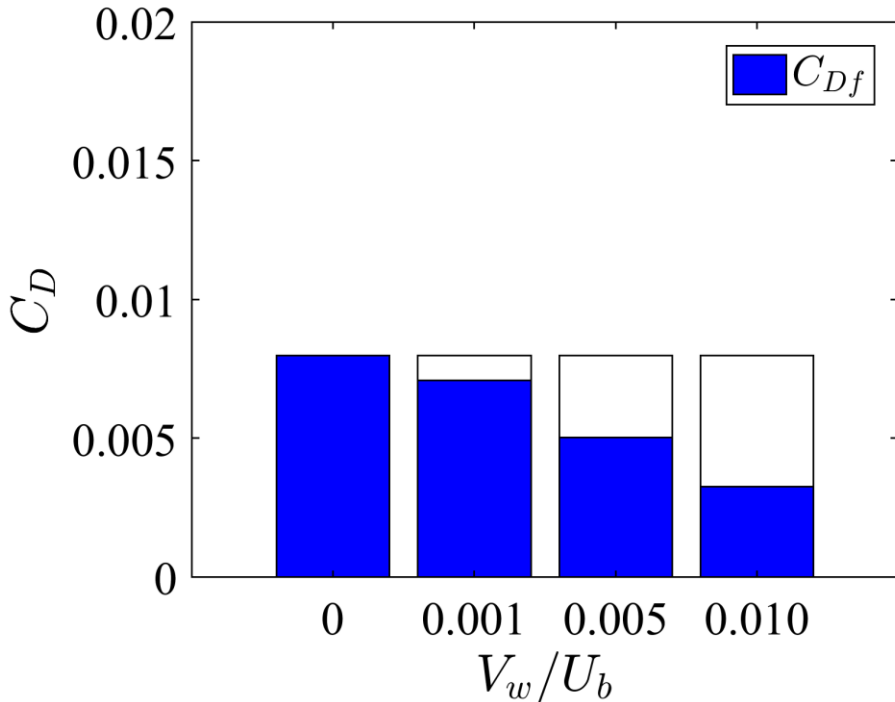
$$C_{Dp} = 2C_{Dave} - (C_{Df} + C_{Df,u})$$

C_{Dave} : Overall drag coefficient
 C_{Df} : C_f of the rough wall side
 $C_{Df,u}$: C_f of the smooth wall side

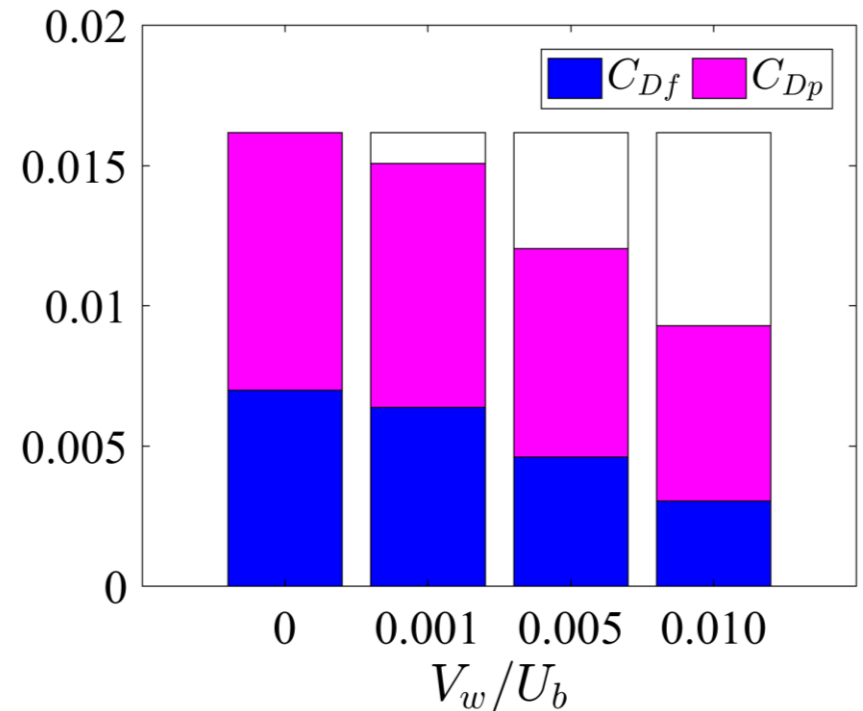
“Transitionally-rough regime”

The result of UB

SMOOTH CASE



ROUGH CASE



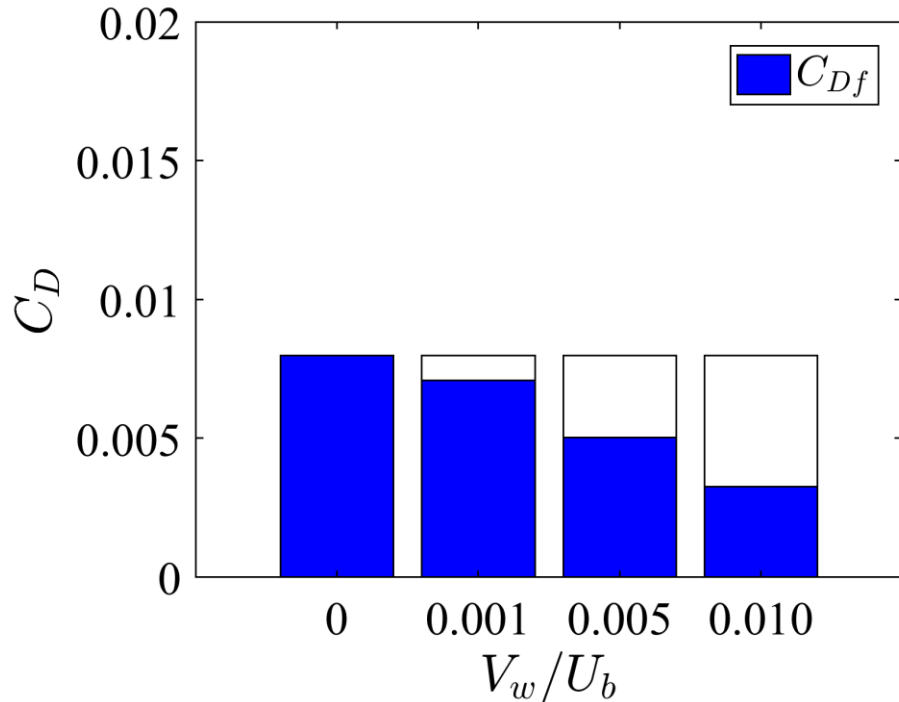
Total, R 11% 37% 59%

7% 26% 43%

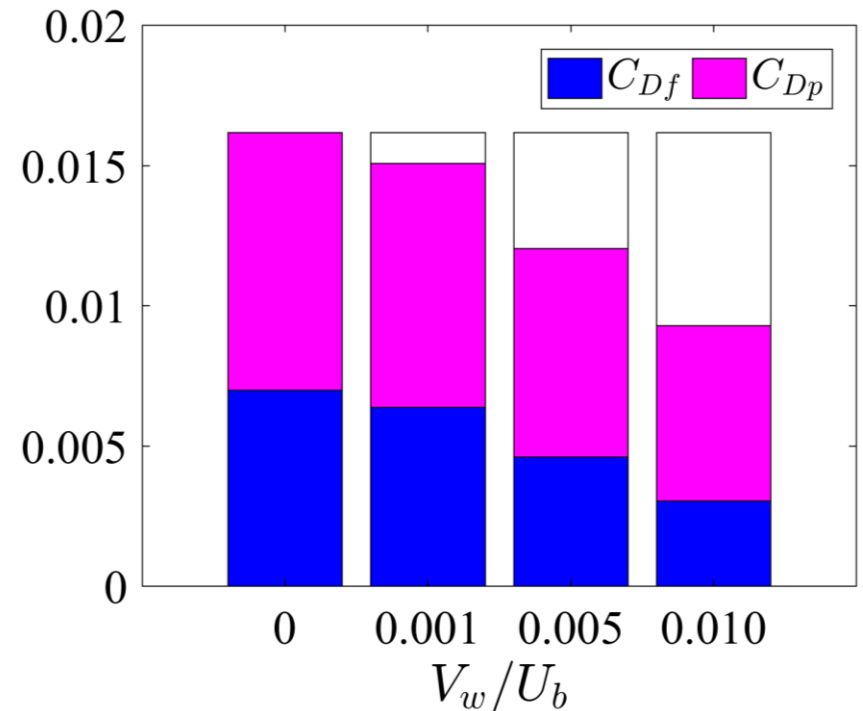
$$R = 1 - \frac{C_{D,ctr}}{C_{D,nc}} \quad \begin{array}{l} C_{D,ctr}: \text{controlled} \\ C_{D,nc}: \text{no control} \end{array}$$

The result of UB

SMOOTH CASE



ROUGH CASE

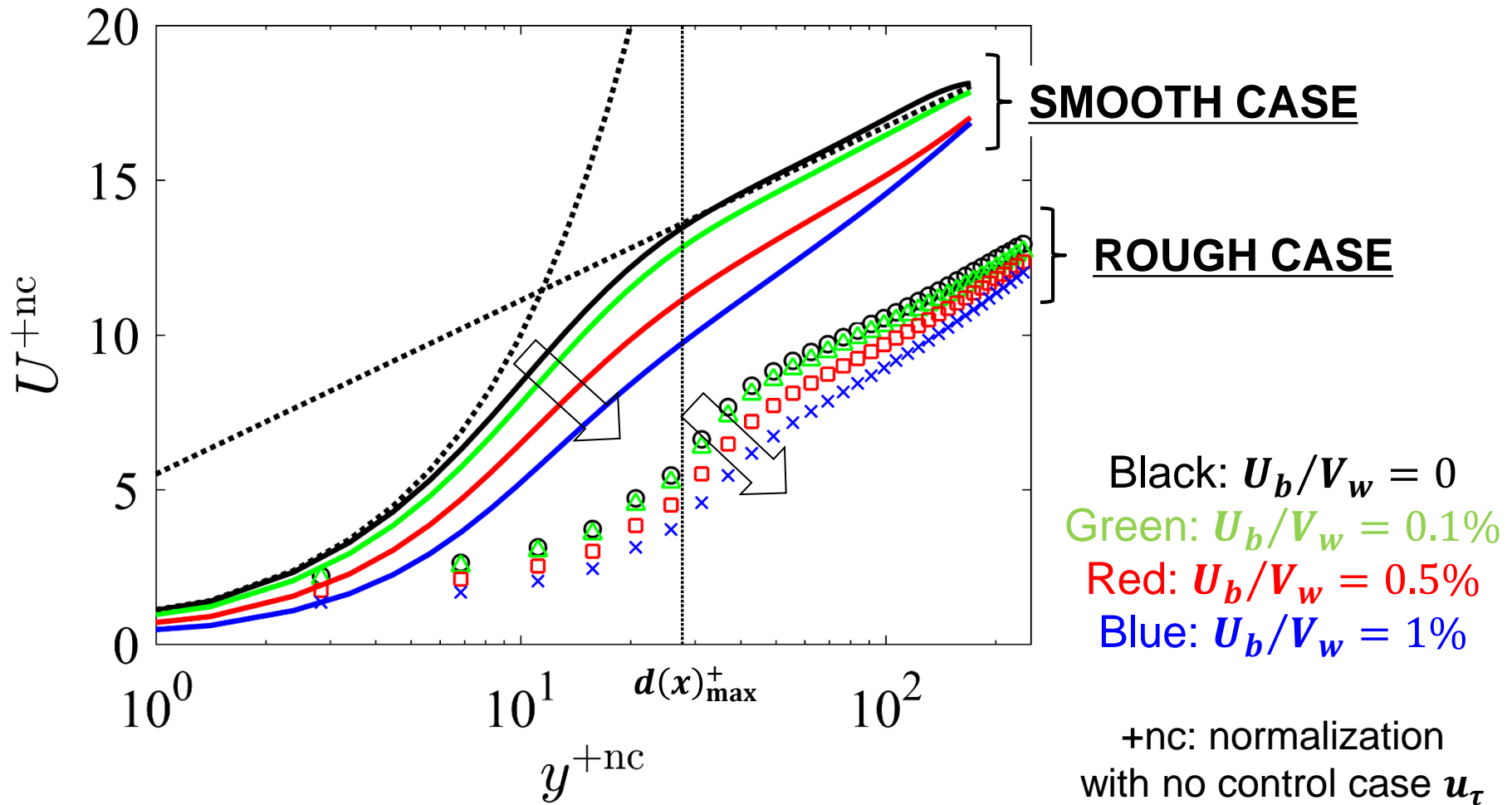


Total, R **11% 37% 59%**
Friction, R_F **11% 37% 59%**
Pressure, R_P - -

7% 26% 43%
9% 34% 57%
5% 19% 32%

Friction drag reduction mechanism

Bulk mean streamwise velocity

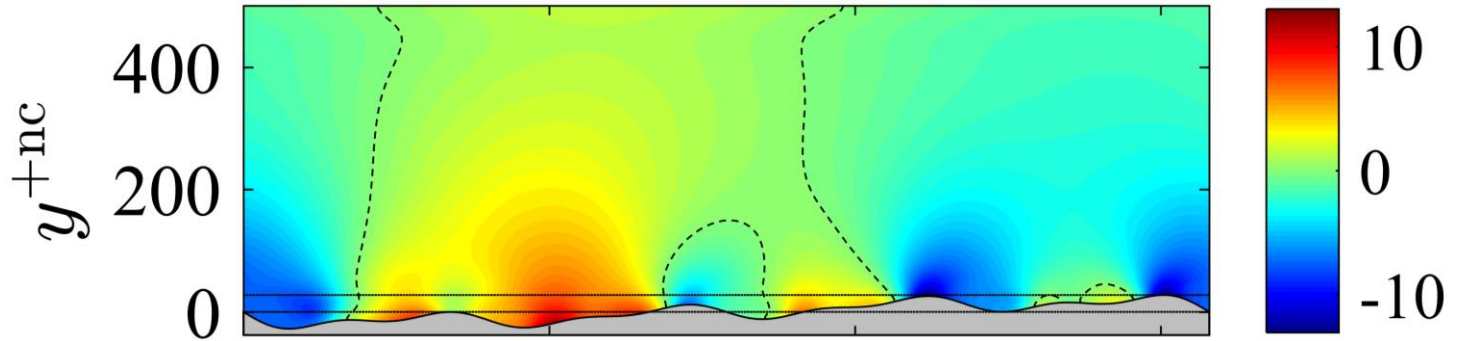


How does pressure drag decrease?

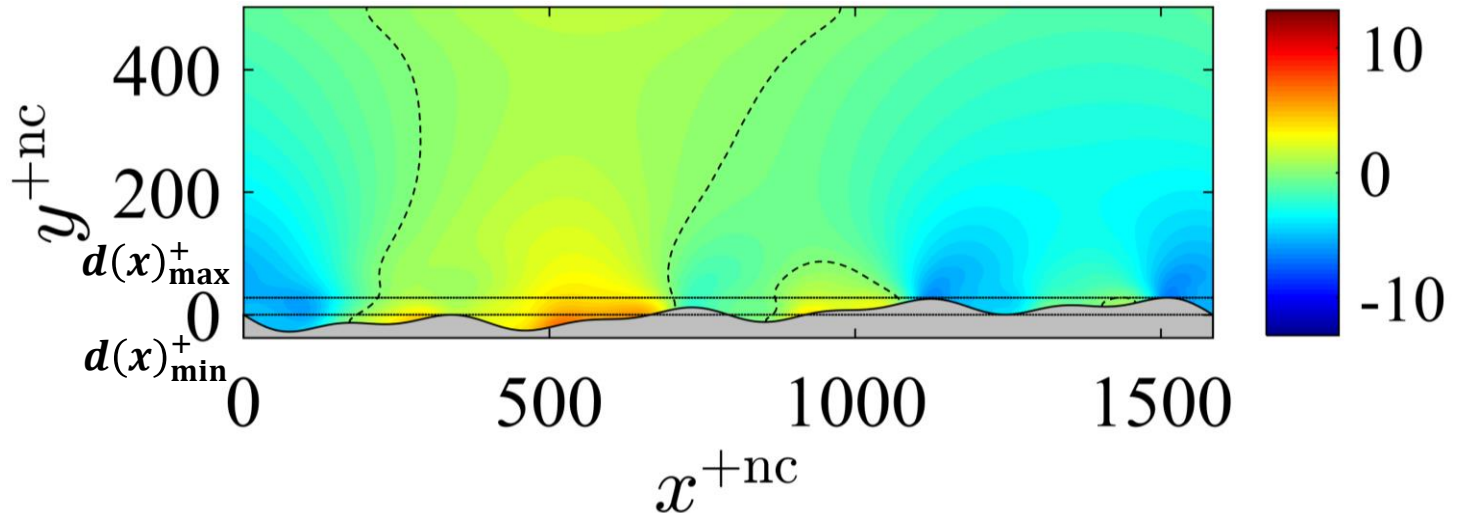
Pressure contours

averaged in the spanwise and time
dashed lines: zero contour
 p^{+nc}

$$U_b/V_w = 0$$



$$U_b/V_w = 1\%$$

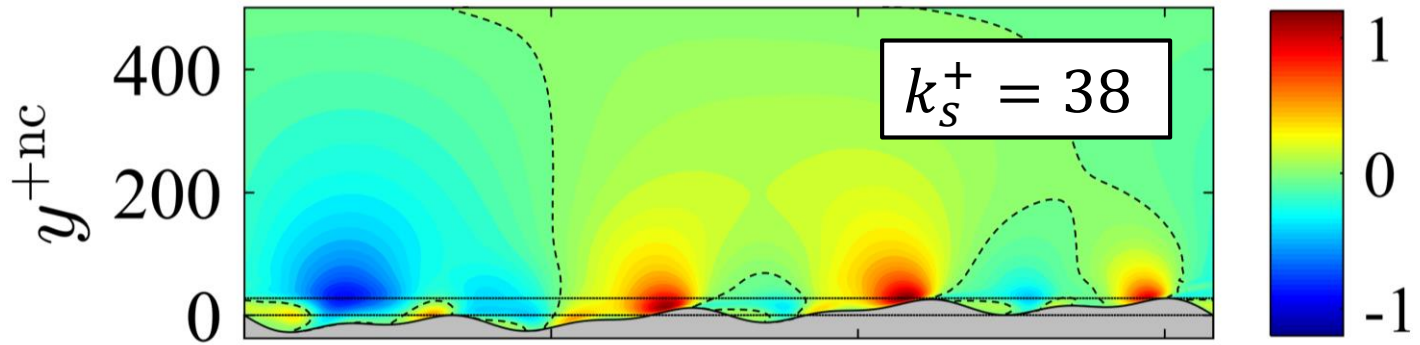


“Smoothing effect”

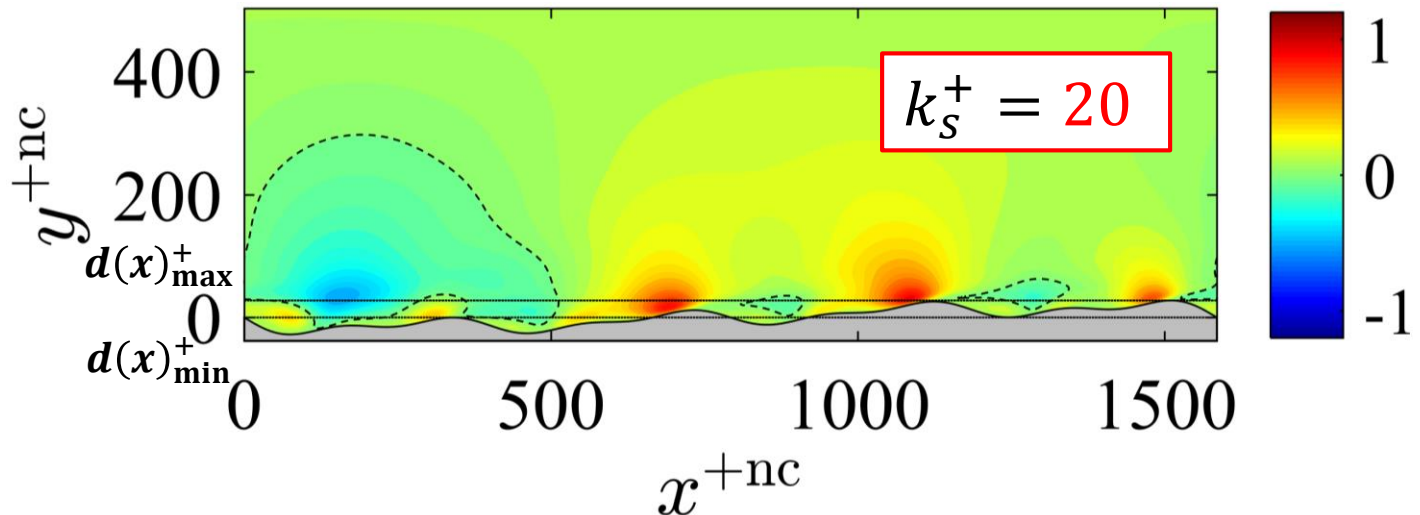
Wall-normal velocity contours

averaged in the spanwise and time
dashed lines: zero contour
 v^{+nc}

$$U_b/V_w = 0$$

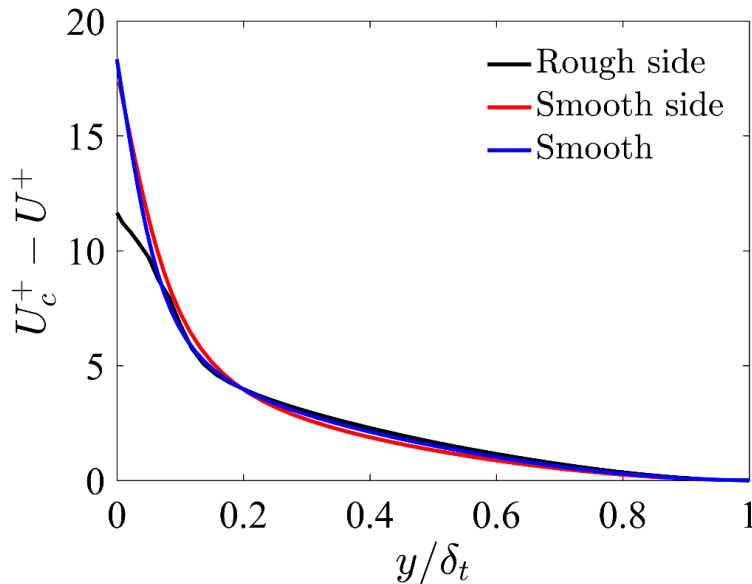


$$U_b/V_w = 1\%$$

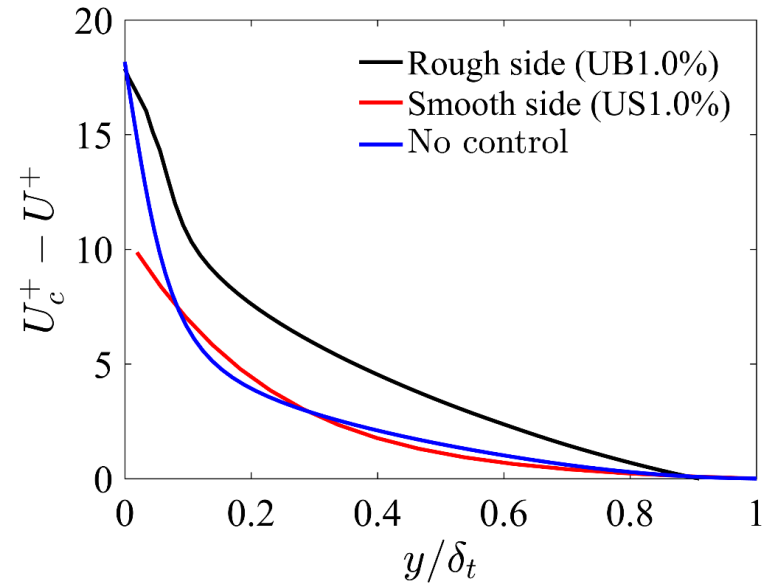


Outer layer similarity with UB

Velocity defect



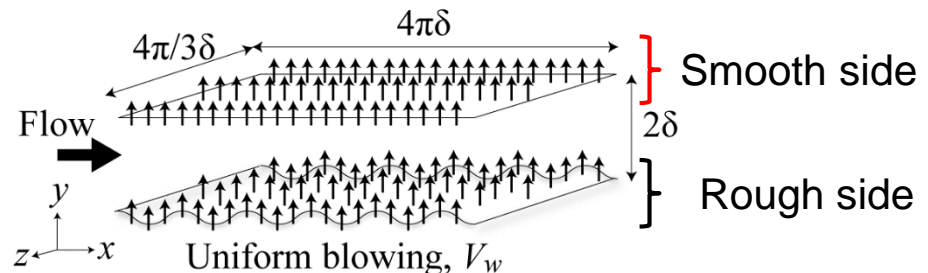
Base flow (No controlled) of one-side rough wall



1% UB case of one-side rough wall

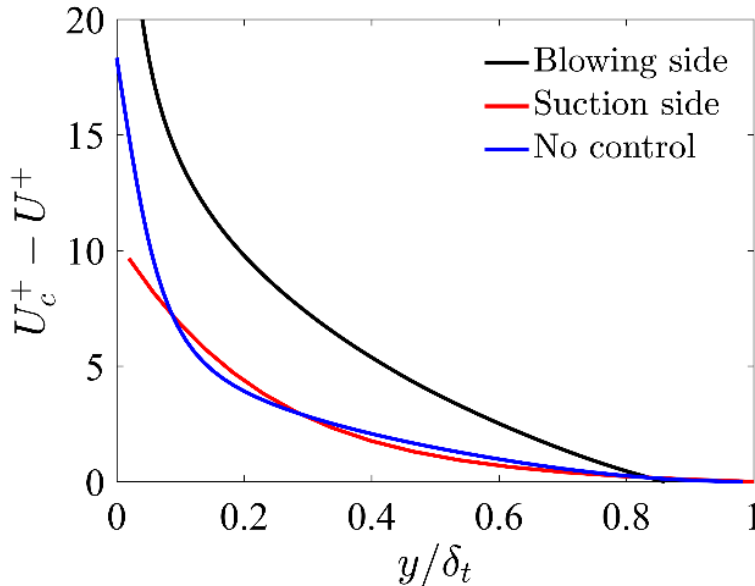
δ_t : distance from a wall to the minimum RMS location

(K. Bhaganagar et al., *Flow, Turbul. Combust.*, 2004)

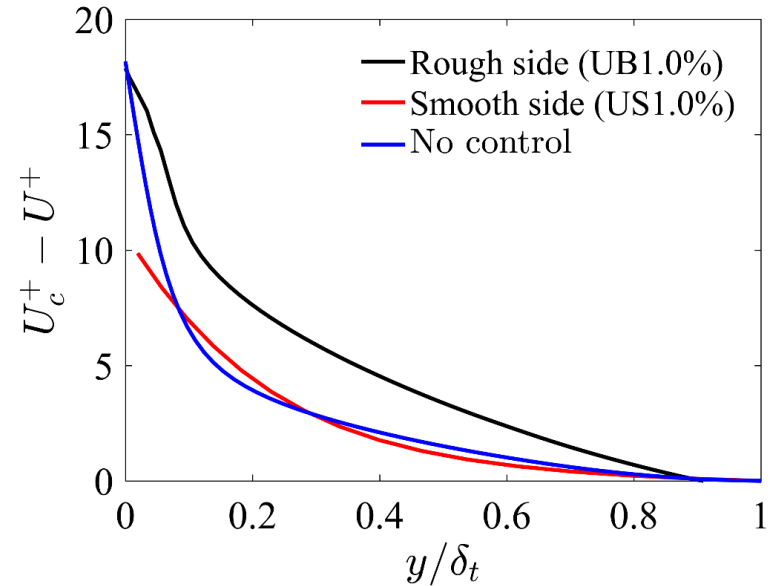
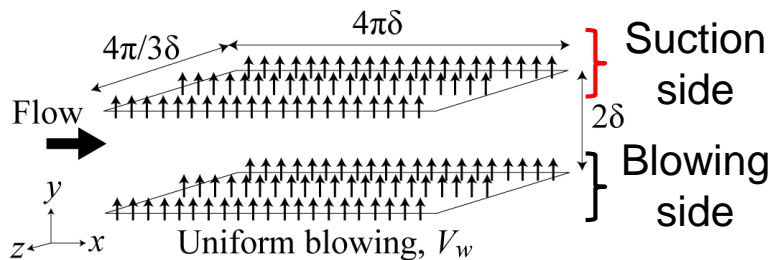


Comparison with smooth case

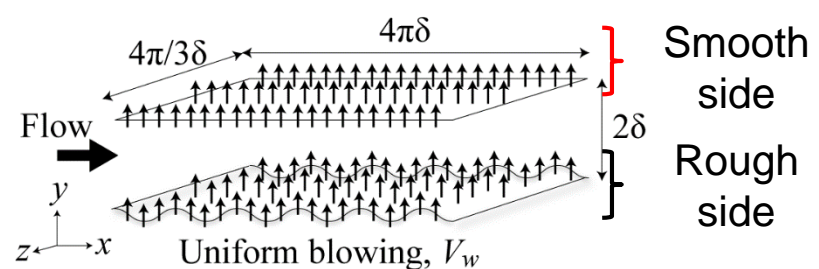
Velocity defect



1% UB case of
both-side smooth wall

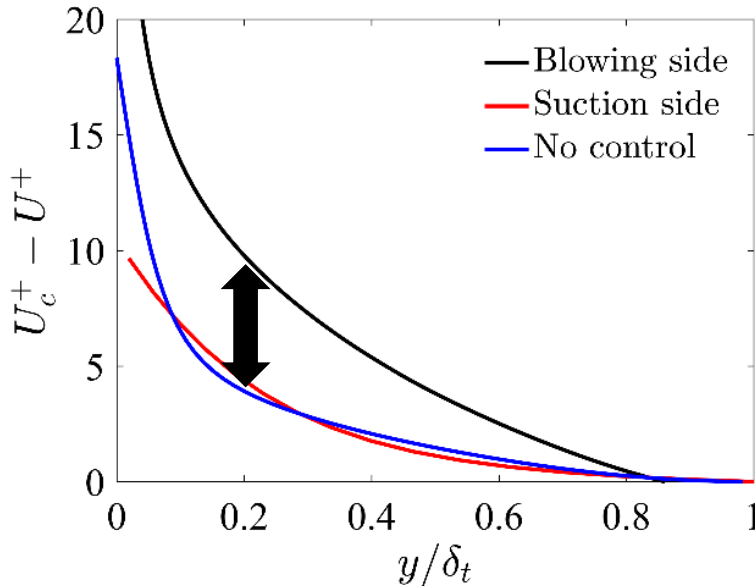


1% UB case of
one-side rough wall

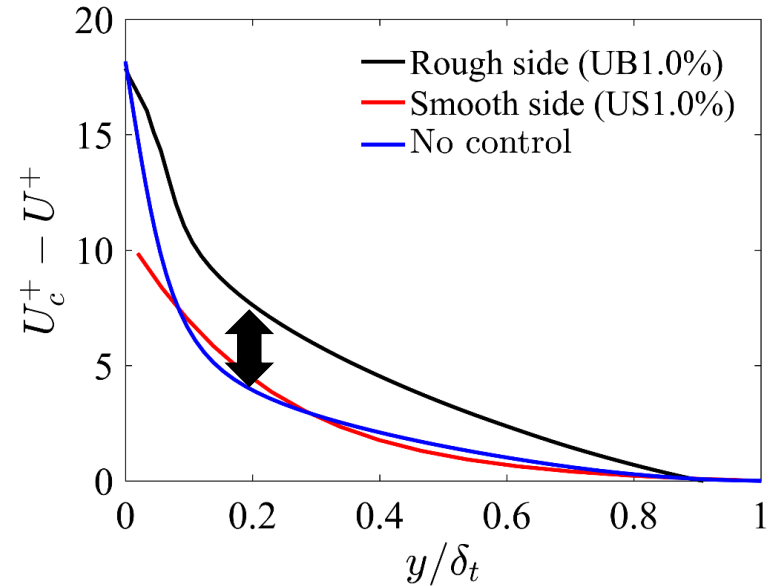


Comparison with smooth case

Velocity defect



1% UB case of
both-side smooth wall



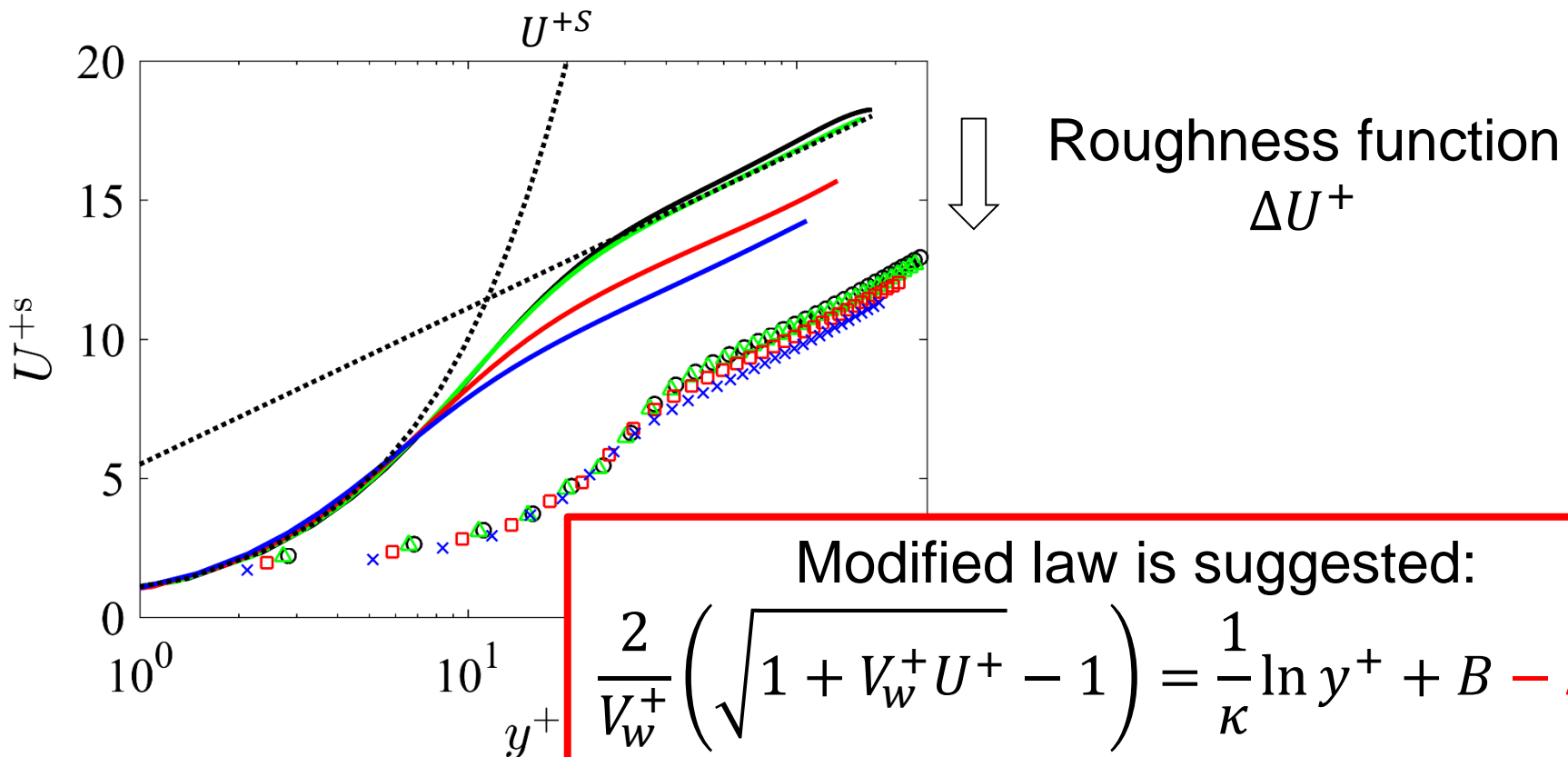
1% UB case of
one-side rough wall

Same tendency, but quantitatively weakened

Stevenson's law of the wall

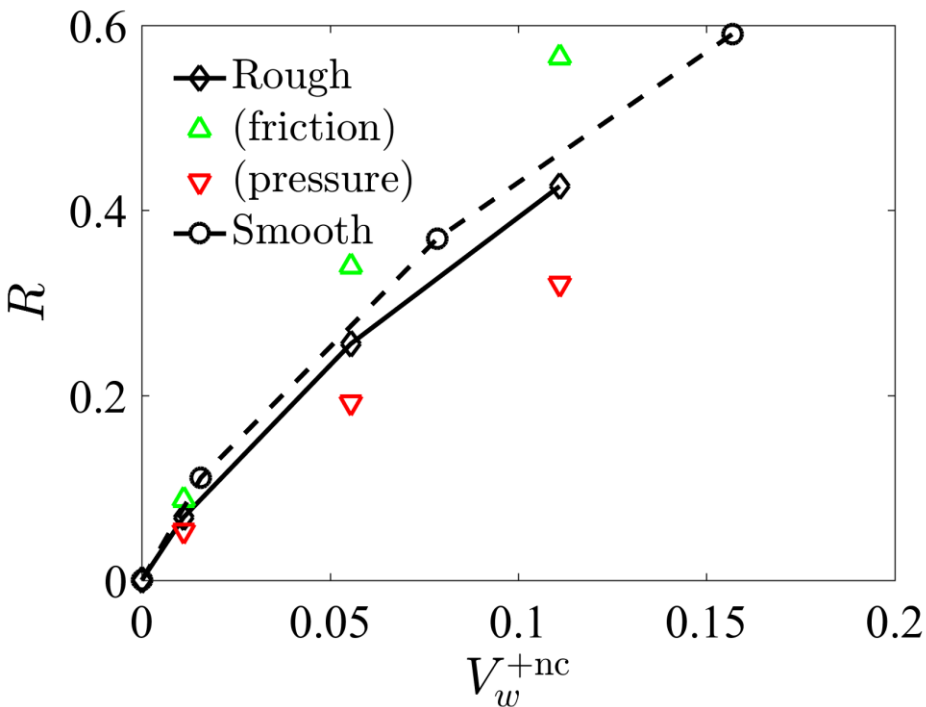
Plots using Stevenson's law of the wall (Stevenson, 1963)

$$\underbrace{\frac{2}{V_w^+} \left(\sqrt{1 + V_w^+ U^+} - 1 \right)}_{U^{+s}} = \frac{1}{\kappa} \ln y^+ + B$$

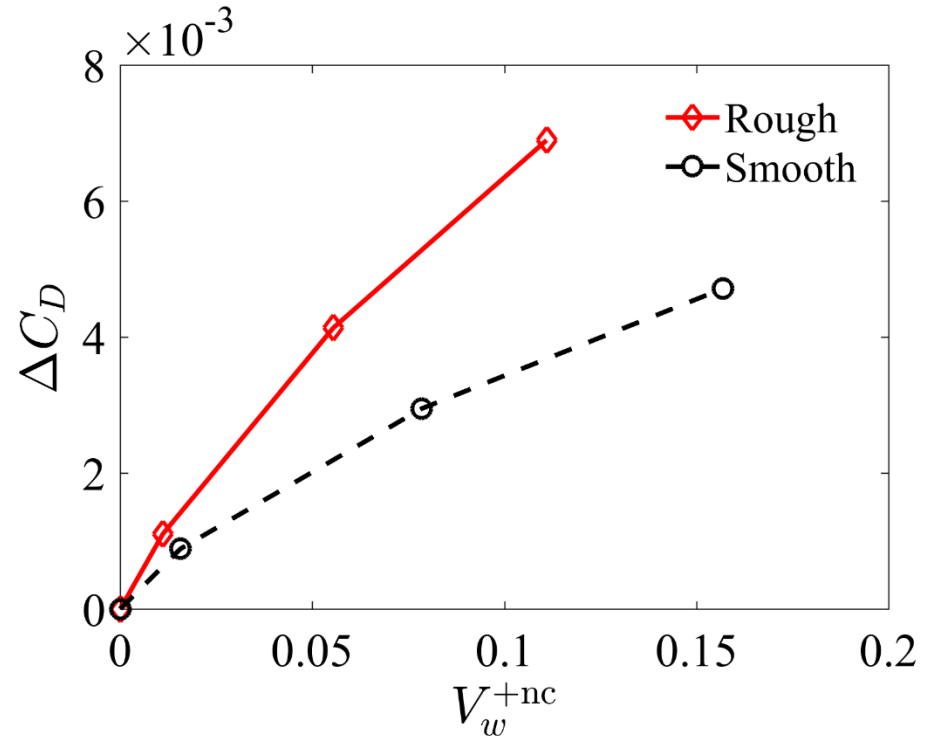


Normalization by u_τ^{nc+}

Drag reduction rate,
 R



Drag reduction,
 $\Delta C_D = C_{D,nc} - C_{D,ctr}$



R becomes similar when plotted with V_w^{+}

nc: no control
ctr: controlled

Concluding remarks

DNS of turbulent channel flow is performed over a rough wall with UB

- **UB is effective over a rough wall**
 - Almost same in drag reduction rate, but larger in drag reduction amount (when normalized by u_{τ}^{+nc})
- **Drag reduction mechanisms are considered**
 - Friction drag is reduced by wall-normal convection
 - Pressure drag is reduced by “smoothing effect”
- **Combined effect (UB + roughness) slightly exists**
- **Modified Stevenson’s law of the wall is suggested**

Thank you for your kind attention

Background

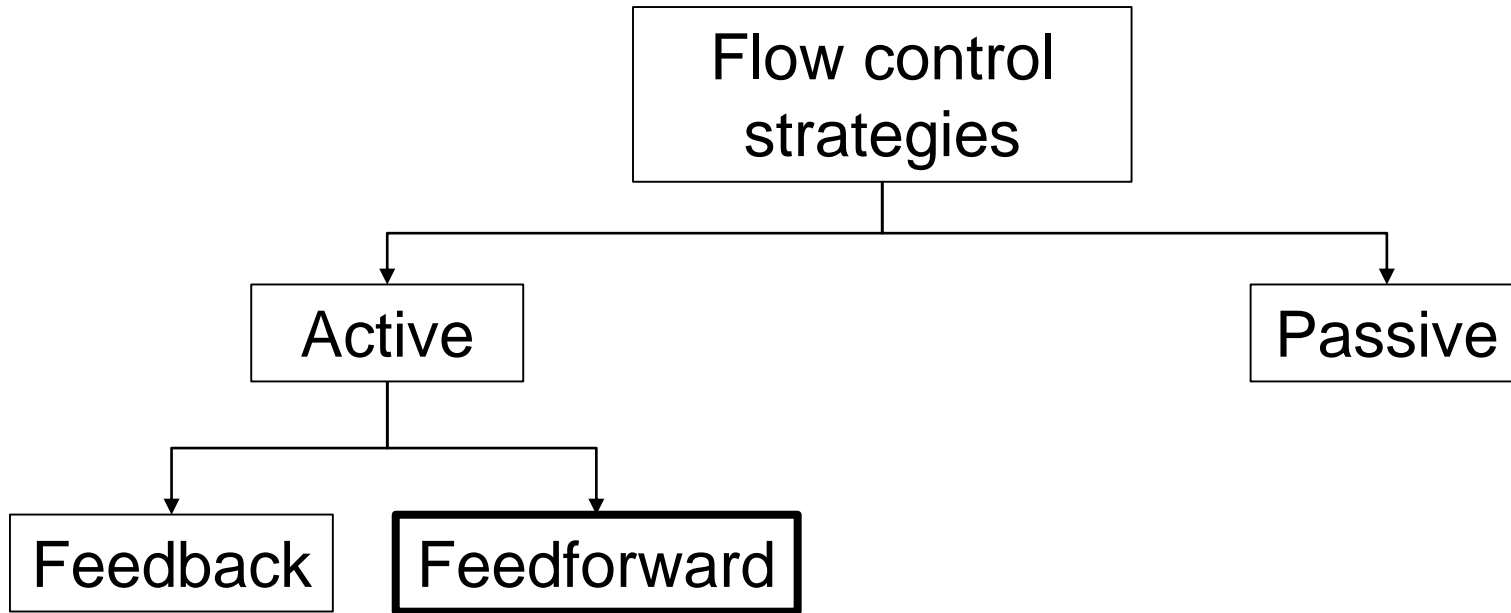
Turbulence

- **Huge drag**
- **Environmental** problems
- High operation **cost**
- **How to control?**



Flow control classification

(M. Gad-el-Hak, *J. Aircraft*, 2001)



- Uniform blowing

Governing equations

(S. Kang & H. Choi, *Phys. Fluids*, 2000)

Incompressible Continuity and Navier-Stokes in ξ_i coordinate

$$\left\{ \begin{array}{l} \frac{\partial u_i}{\partial \xi_i} = -S \\ \frac{\partial u_i}{\partial t} = -\frac{\partial(u_i u_j)}{\partial \xi_j} - \frac{\partial p}{\partial \xi_i} + \frac{1}{\text{Re}_b} \frac{\partial^2 u_i}{\partial \xi_j \partial \xi_j} - \frac{dP}{d\xi_1} \delta_{i1} + S_i \end{array} \right.$$

where

$$S_i = -\varphi_t \frac{\partial u_i}{\partial \xi_2} - \phi_j \frac{\partial(u_i u_j)}{\partial \xi_2} - \phi_j \frac{dp}{d\xi_2} \delta_{ij} + \frac{1}{\text{Re}} \left(2\phi_j \frac{\partial^2 u_i}{\partial \xi_j \partial \xi_2} + \phi_j \phi_j \frac{\partial^2 u_i}{\partial \xi_2^2} + \frac{1}{2} \frac{\partial(\phi_j \phi_j)}{\partial \xi_2} \frac{\partial u_i}{\partial \xi_2} \right)$$

$$S = \phi_j \frac{\partial u_i}{\partial \xi_2} \quad \phi_j = \varphi_j - \delta_{j2} \quad \varphi_j = \begin{cases} -\frac{1}{1+\eta} \left(\xi_2 \frac{\partial \eta}{\partial \xi_i} + \frac{\partial \eta_0}{\partial \xi_i} \right), & \text{for } j = 1, 3 \\ \frac{1}{1+\eta}, & \text{for } j = 2 \end{cases}$$

Coordinate transformation

(S. Kang & H. Choi, *Phys. Fluids*, 2000)

Calculation grids: ξ_i (Cartesian with extra force)

$$\begin{cases} x = \xi_1 \\ y = \xi_2(1 + \eta) + \eta_d \\ z = \xi_3 \end{cases}$$

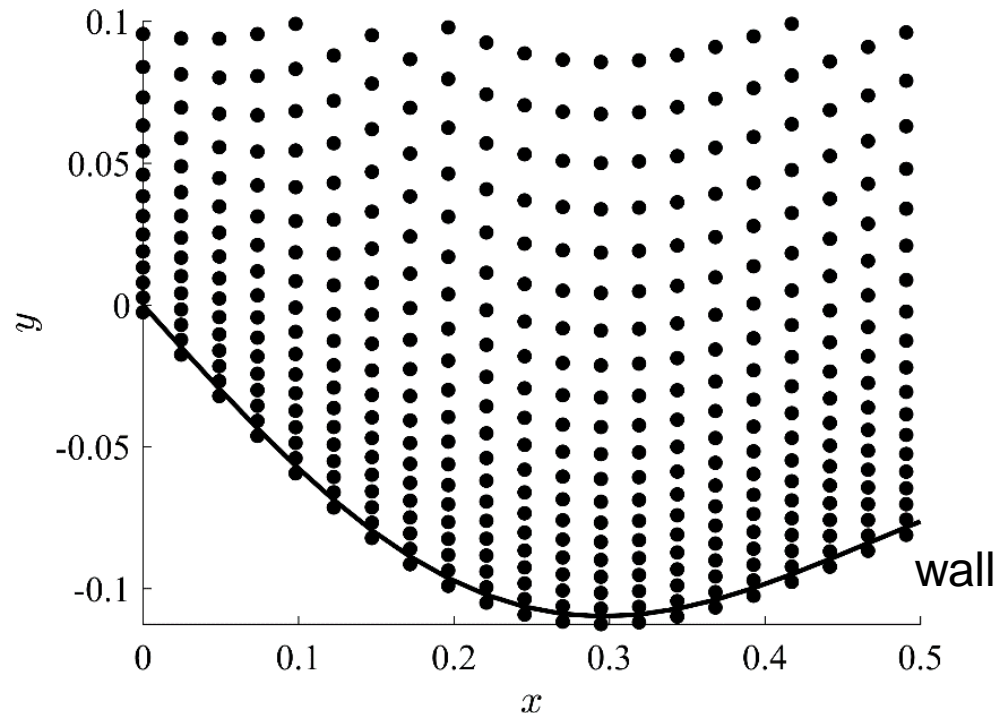
(x, y, z : physical coordinate)

$$\begin{aligned} \eta &\equiv (\eta_u - \eta_d)/2 \\ &= -d(x)/2 \end{aligned}$$

$$\eta_d = r(x), \eta_u = 0$$

η_d, η_u : displacement of
lower/upper wall

Actual grid points allocation



Post processing

- Drag coefficient decomposition for rough case

$$C_{Duf} = \frac{8}{Re_b} \frac{d\bar{u}}{dy} \Big|_{\xi_2=2}$$

$$C_{Dlf} = \frac{8}{Re_b} \left(\frac{du}{dy} \Big|_{\xi_2=0} + \frac{dv}{dx} \Big|_{\xi_2=0} \right)$$

(Friction component)

$$C_{Dlp} = -16 \frac{dP}{d\xi_1} - (C_{Dlf} + C_{Duf})$$

(Pressure component)

- Drag reduction rate

$$R_{Dl} = \frac{\Delta C_D}{C_{D,M=0}} \times 100 [\%]$$

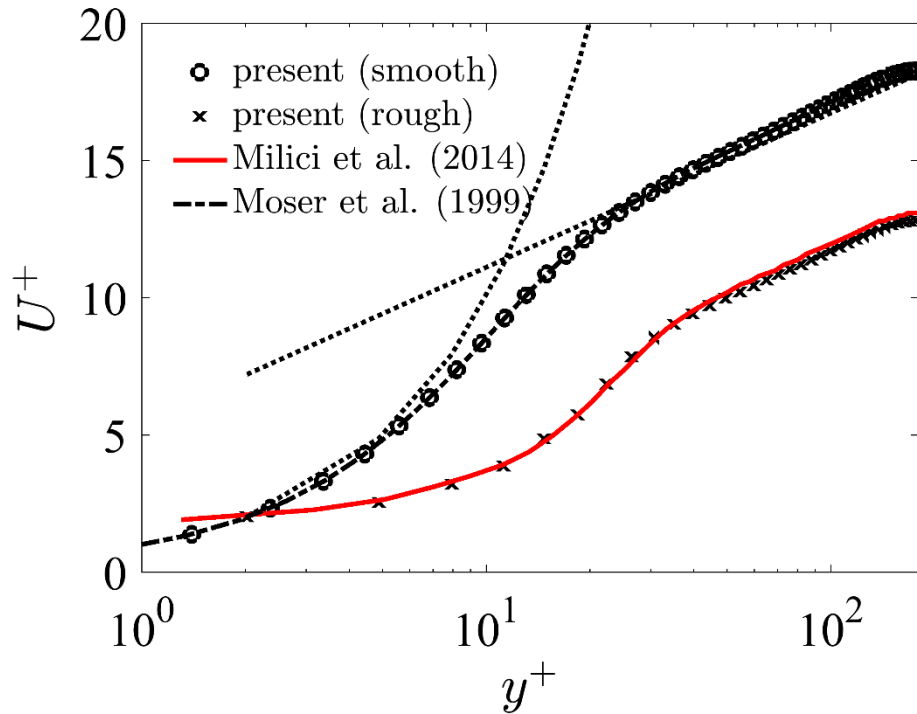
Only focusing on lower side,
subscript “l” omitted hereafter

Discretization methods

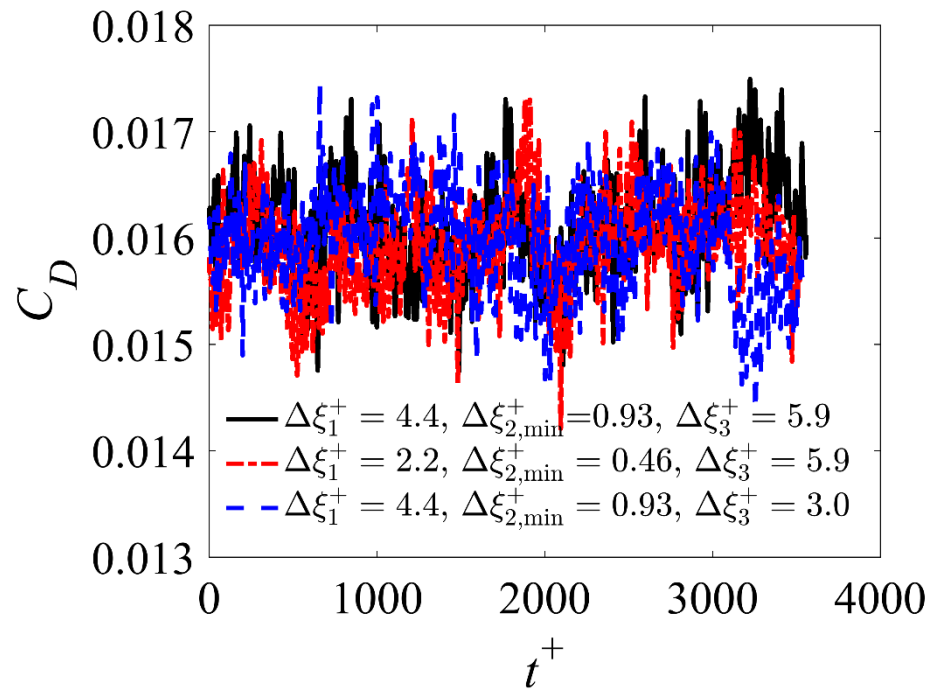
- **Energy-conservative second-order finite difference schemes (In space)**
- **Low-storage third-order Runge-Kutta / Crank-Nicolson scheme (In time)**
 - + **SMAC method for pressure correction**

Discretized in the staggered grid system

Validation & Verification



Bulk mean streamwise velocity



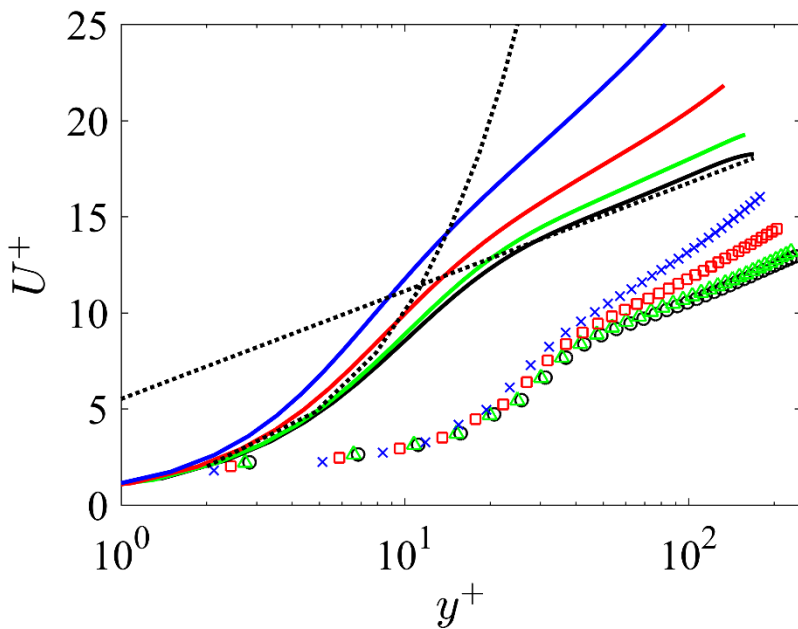
Time trace of instantaneous C_D

*Less than 2% of difference
from the most resolved case*

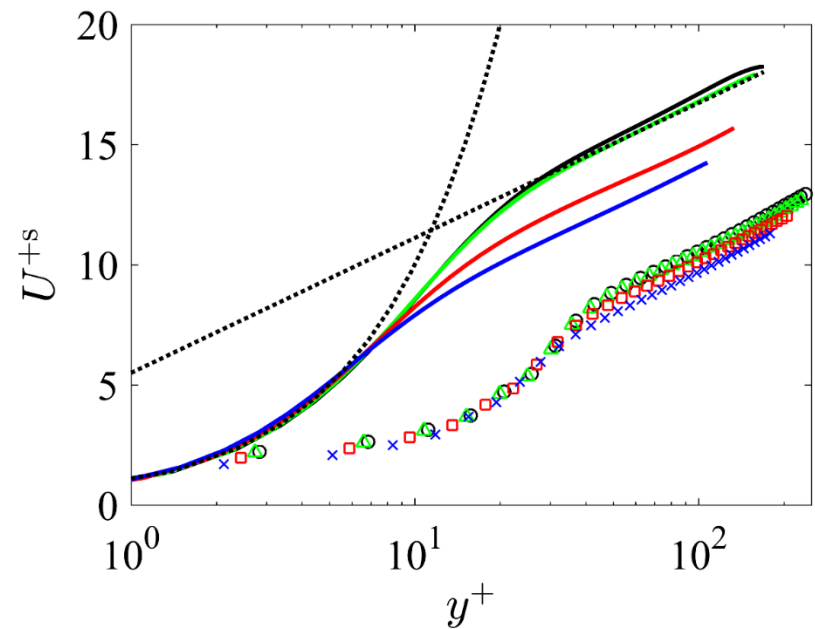
Stevenson's law of the wall

Plots using Stevenson's law of the wall (Stevenson, 1963)

$$\underbrace{\frac{2}{V_w^+} \left(\sqrt{1 + V_w^+ U^+} - 1 \right)}_{U^{+s}} = \frac{1}{\kappa} \ln y^+ + B$$



Normalized by local u_τ



Normalized by Stevenson's law