## Direct numerical simulation

### of turbulent flow

## in an annular pipe

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- plane channel flow (adapt a computer code without structural changes) Extend to the cylindrical geometry a numerical method for the DNS of turbulent
- Perform DNS of the turbulent flow in an annular pipe (never reported)

## What is DNS of turbulence?

Numerical solution of the full Navier–Stokes equations (vs. LES or RANS)

- Full range of spatial & temporal scales in turbulent flows needs to be accounted for
- Requirements of spatio-temporal resolution rise with Re
- ightarrow DNS of practical flows at high Re is unaffordable
- Research tool, suited for basic turbulence research (flow physics, turbulence modeling)
- Very demanding in terms of computational resources, even at low/moderate Re

# **DNS** of turbulence in cylindrical coordinates

- Numerical difficulties of cylindrical coordinate system
- ightarrow few DNS of turbulent flow in cylindrical geometries (pipe flow only)
- Many of the numerical schemes solve NS eqs in primitive variables, with the pressure-correction approach
- Only one DNS study (Neves, Moin & Moser, JFM v.272, 1994) considers cylinders (with insufficient resolution in the outer part of the layer) transverse curvature, but is concerned with the boundary layer over small
- The comparison between the effects of convex / concave transversal curvature on the turbulence statistics is still missing

## The (standard) cartesian case

Moin & Moser (JFM v.177, 1987), by which: For plane channel flow, there is an almost standard procedure developed by Kim,

- Pressure is eliminated from the equations
- NS system is reduced to a second-order scalar equation for the normal vorticity and a fourth-order scalar equation for the normal velocity
- When using Fourier transforms in homogeneous directions, the other velocity components are easily recovered
- High (nearly optimal) computational efficiency can be achieved



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component, one obtains for  $\omega_y = \partial u/\partial z - \partial w/\partial x$ : By applying  ${f 
abla} imes$  to the momentum equation,  ${f 
abla} imes {f 
abla} p = 0$ . Considering the yBy manipulating momentum equation, and using continuity, one obtains for v: Initial conditions. Periodicity in x and z. No-slip boundary conditions at the walls:  $\frac{\partial}{\partial t} \nabla^2 v = \frac{1}{Re} \nabla^4 v + \left( \frac{\partial^2}{\partial x^2} + \frac{\partial^2}{\partial z^2} \right) H_v - \frac{\partial}{\partial y} \left( \frac{\partial}{\partial x} H_u + \frac{\partial}{\partial z} H_w \right)$  $v(x, z, \pm \delta) = 0; \quad v_y(x, z, \pm \delta) = 0; \quad \omega_y(x, z, \pm \delta) = 0$  $\frac{\partial}{\partial t}\omega_y = \frac{1}{Re}\nabla^2 \omega_y + \frac{\partial H_u}{\partial z}$ Cartesian case (cont.)  $\partial H_w$  $\partial x$ 



Partially implicit approach is very popular: explicit schemes for the wide range of spatial scales

Implicit time schemes are usually not used, due to the need of accuracy over a

convective part, but implicit schemes for the viscous terms (with time-scales

smaller than those needing accurate representation)

	Cylindrical case
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$\partial u = 1 \partial (rv) = 1 \partial w$	$\begin{array}{c} \textbf{Cylindrical case}\\ \partial u & 1 \partial (rv) & 1 \partial w \end{array}$
$\partial u = 1 \partial (rv) = 1 \partial w$	$\begin{array}{c} \textbf{Cylindrical case}\\ \partial u & 1 \partial (rv) & 1 \partial w \\ 0 \end{array}$
$\frac{\partial u}{\partial u} + \frac{1}{2} \frac{\partial (rv)}{\partial u} + \frac{1}{2} \frac{\partial w}{\partial u} = 0$	$\frac{\partial u}{\partial u} \pm \frac{1}{2} \frac{\partial (rv)}{\partial u} \pm \frac{1}{2} \frac{\partial w}{\partial u} = 0$
$\frac{\partial u}{\partial x} + \frac{1}{2} \frac{\partial (rv)}{\partial x} + \frac{1}{2} \frac{\partial w}{\partial x} = 0$	$\frac{\partial u}{\partial u} + \frac{1}{2} \frac{\partial (rv)}{\partial v} + \frac{1}{2} \frac{\partial w}{\partial v} = 0$
$\frac{\partial u}{\partial x} + \frac{1}{2} \frac{\partial (rv)}{\partial x} + \frac{1}{2} \frac{\partial w}{\partial x} = 0$	$\frac{\partial u}{\partial w} + \frac{1}{2} \frac{\partial (rv)}{\partial w} + \frac{1}{2} \frac{\partial w}{\partial w} = 0$
$\frac{\partial u}{\partial w} + \frac{1}{2} \frac{\partial (rv)}{\partial w} + \frac{1}{2} \frac{\partial w}{\partial w} = 0$	$\frac{\partial u}{\partial w} + \frac{1}{2} \frac{\partial (rv)}{\partial w} + \frac{1}{2} \frac{\partial w}{\partial w} = 0$
$\frac{\partial u}{\partial m} + \frac{1}{m} \frac{\partial (rv)}{\partial m} + \frac{1}{m} \frac{\partial w}{\partial h} = 0$	$\frac{\partial u}{\partial m} + \frac{1}{m} \frac{\partial (rv)}{\partial m} + \frac{1}{m} \frac{\partial w}{\partial h} = 0$
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$\frac{\partial u}{\partial x} + \frac{1}{r}\frac{\partial (rv)}{\partial r} + \frac{1}{r}\frac{\partial w}{\partial \theta} = 0$ $\frac{\partial u}{\partial t} + u\frac{\partial u}{\partial x} + v\frac{\partial u}{\partial r} + \frac{w}{r}\frac{\partial u}{\partial \theta} = -\frac{\partial p}{\partial x} + \frac{1}{Re}\nabla^2 u$	$\begin{aligned} \begin{array}{l} \textbf{Cylindrical case} \\ \hline \boldsymbol{\partial} u \\ \frac{\partial u}{\partial x} + \frac{1}{r} \frac{\partial (rv)}{\partial r} + \frac{1}{r} \frac{\partial w}{\partial \theta} = 0 \\ \hline \frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial r} + \frac{w}{r} \frac{\partial u}{\partial \theta} = -\frac{\partial p}{\partial x} + \frac{1}{Re} \nabla^2 u \end{aligned}$
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### Cylindrical case (cont.)

lpha) and heta (wave number m) these difficulties are left: By Fourier transforming the equations in homogeneous directions x (wave number

- impossible implicit treatment of viscous terms: components of the momentum equation are coupled
- $k^2=lpha^2+m^2/r^2$  depends on r!

Notation:

$$Df = \frac{\partial f}{\partial r}; \quad D_*f = \frac{\partial f}{\partial r} + \frac{f}{r} \quad \Rightarrow \nabla^2 = -k^2 + D_*D$$



considering the r component, one obtains for radial vorticity  $\eta$ : In analogy with the cartesian case, by taking  ${oldsymbol 
abla} imes$  of the momentum equation and

$$\frac{\partial \hat{\eta}}{\partial t} = \frac{1}{Re} \left( \nabla^2 \hat{\eta} - \frac{\hat{\eta}}{r^2} + 2\frac{im}{r^2}D\hat{u} + 2\frac{m\alpha}{r^2}\hat{v} \right) + \frac{im}{r}\hat{H}_u - i\alpha\hat{H}_w$$

- Not independent of  $\hat{v}$  anymore (no problem if equation for  $\hat{v}$  does not contain  $\hat{\eta}!$ )
- Contains a curvature term  $\sim D \hat{u}$
- Both  $\hat{v}$  and  $\hat{u}$  terms can enter the explicit part: low-order derivatives, presumably small since difference with cartesian, hence no stability problems





### The numerical solution

- space; De-aliasing with the 3/2 rule. FFT algorithms allow exact computation of the nonlinear terms in physical
- Radial derivatives discretized with finite differences over a 5-point stencil; scheme low-order derivatives are IV order, higher order derivatives are IInd order ightarrow formally lind order method, but advantageous compared to a lind order
- second-order Crank-Nicholson for the implicit part. Time integration: as in KMM, third-order Runge-Kutta for the explicit part, and



- Periodicity assumption in x and heta directions
- Inner radius  $\mathcal{R}_i = 2\delta$  and outer radius  $\mathcal{R}_o = 4\delta$ ; gap  $\mathcal{R}_o \mathcal{R}_i = 2\delta$
- $lpha_0=0.5$  which gives  $L_x=4\pi\delta$

 $m_0=2$  which gives  $2\pi\delta\leq L_ heta\leq 4\pi\delta$  (inner / outer walls)

- No need to consider full circumferential extension of the annulus:  $m_0=2$  gives spanwise dimensions wider than plane case
- $Re = U_b \delta / 
  u = 2800$ , where  $U_b$  is bulk velocity; corresponds to  $Re_ au \sim 184$ value for channel flow) for the inner wall, and  $Re_{ au}=176$  for the outer wall ( $Re_{ au}=180$  reference
- Constant flow rate; after reaching steady state, computations are carried out for  $150 \; t U_b/\delta$ , storing flow fields every  $15 \; t U_b/\delta$

# Transversal resolution & cylindrical coordinates

- For a given  $m_0$ , transversal size of the computational domain increases with r
- Physical considerations dictate minimal required resolution, needed at outer wall
- Resolution increases (linearly) above necessary approaching inner wall
- $\Rightarrow$  potential stability problems, and waste of computational resources
- With Fourier schemes, Fourier series must be truncated at wavenumber corresponding to maximum resolution

#### Solution

An r-dependent truncation of the series can remove the unneeded azimuthal

modes, saving memory and CPU time, and avoiding stability problems

## **Computational parameters**

- Radial range divided in 128 (uneven) intervals
- 193 Fourier modes in axial direction:  $-96 \leq lpha/lpha_0 \leq +96$
- 321 Fourier modes in  $\theta$  direction at  $r = \mathcal{R}_o$ :  $-160 \leq m/m_0 \leq +160$ ; they linearly reduce to 161 at  $r = \mathcal{R}_i$
- Spatial resolution is very high:  $\Delta x^+ \sim 11.7; \Delta z^+ \sim 5.8; \Delta r^+ = 0.9 4.5$
- 12 millions d.o.f.; RAM memory: 310MB; single flow field on disk: 110MB
- 280 seconds / time step for a SMP personal computer (2 CPU Intel 550MHz); parallel speedup of 100%
- Time step  $0.02 \ t U_b/\delta$  (comparable to planar case); computing time  $\sim$  3 weeks







#### Conclusions

- been presented, as an extension of the cartesian case An efficient method for DNS of turbulent flows in cylindrical geometries has
- The number of Fourier modes in  $\theta$  direction has been varied with r, so that the azimuthal resolution is constant: significant benefits
- Turbulent flow in the annular pipe has been studied for the first time via DNS
- curvature on the turbulence statistics have been reported Preliminary observations on the effect of the transverse (concave and convex)